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EVALUATION OF GLUCOSE SYRUP PRODUCED FROM CASSAVA HYDROLYZED WITH MALTED GRAINS (RICE, SORGHUM & MAIZE)

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ABSTRACT: The crude malt obtained from the grains were hydrolyzed with cassava starch to obtain glucose syrup. 94.33% malt was produced from maize, rice had 84.46% malt, while sorghum had 84.97% malt. Glucose syrup yield was greatest using sorghum malt with percentage yield of 75.55%, 52.37% using rice malt, and while maize malt had 48.33 % syrup. Maize sample had highest malt yield but lowest glucose syrup yield showing that glucose syrup yield is in dependent on malt yield but on the quality of amylase produced during malting. Analysis on the glucose syrup obtained gave the following results: moisture content of 13.8%, 14.5%, 15.4%; ash content of 0.02%, 0.04%, 0.01%; carbohydrate 86.47%, 84.76%, 83.01%; total reducing sugar (invert sugar) 85.79%, 83.86%, 82.58%; total soluble (sugar brix) 100°Brix, 110°Brix, 105°Brix for rice, sorghum and maize samples respectively. Dextrose equivalent, viscosity, colour and taste of the end products were also analyzed. Microbial analysis was 2×10^1 , 5×10^1 , 3×10^1 cfu/mL for glucose syrup from rice, sorghum and maize samples respectively with no trace of yeast or mold growth making the glucose syrup fit for consumption.

INTRODUCTION: Grains are small, hard, dry seeds harvested for human or animal consumption. After harvest, dry grains are able to exist for a long time without significant deterioration than other common foods and this durability has made grains well suited to industrial agriculture. Sorghum, millet, maize, rice and wheat are the most important cereals in Nigeria ^{1, 2, 3}.

Glucose syrup is an undiluted aqueous solution of glucose, maltose and other nutritive saccharides obtained from cassava starch.

Starch is a polysaccharide carbohydrate consisting of a large number of glucose units linked by glycosidic bonds ¹. Starch is one of the most valuable and widely occurring carbohydrate reserves in green plants and it is commercially produced from seeds, tubers and roots of plants ^{2, 3}. Starch can be physically, chemically or enzymatically modified and processed into many value added products ^{2, 4, 5, 6}. A suitable and commercial source of starch is Cassava. Cassava, *Manihot esculenta crantz* is a tuberous plant which grows best in tropical and subtropical areas of the

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world all through the year. By virtue of its high starch content and tolerance to drought, it is one of the most essential crops in the tropics with Nigeria being the highest producer in the world^{7,8}. Glucose syrup is an undiluted aqueous solution of glucose, maltose and other nutritive saccharides from edible starch. Currently, glucose syrup is not sufficiently manufactured in Nigeria but most industries make use of it in their operation. Industrially, it is utilized in large quantities in fruit juices, liquors, crystallized fruits, bakery products, confectionery, pharmaceuticals, and brewery products. It is used to improve shelf life, enhance colour, reduce breakage, and maintain crispiness in breakfast cereals. Import formation revealed that in the year 2003, over 800 million naira was used in the importation of glucose syrup in Nigeria⁹.

Glucose syrup is produced by hydrolysis of starch. In the past, hydrolysis of starch was widely carried out using acid. Several researches carried out on acid hydrolysis of starch favour the use of dilute acids such as hydrochloric acid over other acids because its action on starch is mild and produces lesser amount of side products.

However, acid hydrolysis are generally energy intensive, relatively difficult to control, require the use of materials that do not corrode easily, give rise to high colour and salt-ash content (after neutralization)¹⁰. Enzymatic hydrolysis is now largely replacing the acid hydrolysis because it is easy to control, effective even in mild ambient conditions and do not give rise to any by-product. Enzymatic hydrolysis of starch is done with the use of amylase enzyme¹¹. Amylase enzyme breaks the bonds between the molecules of starch to form glucose. The enzyme is found abundantly in animals, plants, fungi etc. Malting is a means being employed to activate this enzyme in plant.

Malting is the process of controlled germination and quick drying of cereal grains before shoot development¹². Malting is done to promote synthesis of hydrolytic enzymes which breaks macro molecules into compounds of low molecular weight of desired characteristics^{13, 14}. For most industrial processes, barley is the most preferred malting grain. However, Nigeria those not locally produce barley. Barley is majorly grown in cooler temperate regions with Russia, Spain, Canada, and

Germany being the top producers^{15, 16}. The selection of any malting grain among other things will however be based on its suitability for processing, yield of desired flavour qualities and good malting characteristics^{17, 18}.

Among the cereals that have high potential as alternative to barley are maize, sorghum and rice. Maize is one the most considered malting grain perhaps because of its abundant supply and relatively low cost¹⁹. Sorghum (*Sorghum bicolor* (L.) Moench) is a tropical cereal grass grown by cultivation. It is produced in almost all the states in Nigeria which is considered the second largest producer of sorghum²⁰. The locally produced rice is available all year round and is known to be highly nutritious. The malt obtained from the locally produced rice will potentially contain much nutrient. This paper considers the use of maize, sorghum and rice of Nigerian origin as grain in view of their malting characteristics and ultimately their ability to hydrolyze locally produced cassava starch to glucose syrup.

MATERIALS AND METHODS:

Collection of Samples: Rice paddy (*oriza sativa*), maize (*Zea mays*), sorghum (*Sorghum Bicolor*) and cassava (*Manihot esculenta Crantz*) were purchased from open market. All the reagents used were of analytical grade from Sigma Chemicals, USA.

Sample Preparation: Dirt and broken kernel were removed from the grains by hand picking. The grains were weighed and washed thoroughly with distilled water. Extraneous (floating materials) were also removed.

Cassava Flour Production: The tubers were peeled, washed and grated. The grated samples were soaked in water for 3 days, after which it was pressed using a muslin cloth to extract starch content. The starch was allowed to settle down, water was decanted and dry white powder was obtained using a Mitchel drier at 100 °C for 24 h. The whole process must not exceed 24 h in order not for fermentation to set in²¹.

Malting Process: The grains were poured in different bowls and washed thoroughly with distilled water. Floating materials were removed from the water surface. 2 liters of distilled water

was measured and poured into the bowls containing the clean grains. The bowls were covered and left for 24 h (steeping). After steeping for 24 h, water was drained off and washed again thoroughly using distilled water. Each grain were poured in perforated bowls for water to drain. They were then tied in jute bags (still in sieve) and left for 7 days. The jute bags were opened every day to sprinkle the grains with water (germination) and to pick

samples every 24 h. These samples were used to analyze for amylase activity. The malted grains were weighed and put in the oven to dry at low temperature of 50 °C for 3 days. After complete drying they were de-rooted by rubbing in between the two palms to get roots off. The rootlets were sieved and weighed. The malt were weighed, milled with a blender into fine powder and stored in a cool dry place.



FIG. 1: MALTED RICE



FIG. 2: MALTED MAIZE



FIG. 3: MALTED SORGHUM

Extraction of Carbohydrate: The carbohydrate content was extracted with 50% methanol which was prepared by mixing methanol and distilled water at a volume ratio 1:1.

Determination of amylase activity of malted grain: This analysis is done on malted grain samples that were taken every 24 h for 168 h (7 days). The samples were milled and extracted with Acetate buffer. 2.0 g of ground malt was stirred in a 250 Erlenmeyer flask containing 100 ml of sodium chloride solution in a water bath at 20 °C and extracted for 60 min. The content was filtered using (whatman fluted filter paper). 1.0 ml of the filtrate was diluted to 100 ml with sodium chloride solution.

The magnetic bars were placed in the test-tubes and place the rack of the tubes in the 45 °C water bath, 1 ml of standard alpha-amylase was added to each tube. 5 ml acetate buffer was added and pre-incubated for 10 min in the water bath at 45 °C with continuous stirring. 1.0 ml of diluted enzymes extract was added to the tubes, after exactly 15 min, 2 ml sodium hydroxide was added to each tube and mixed by inversion. The tubes were allowed to stand for 15 min in a water bath at 20 °C. The absorbance at 620 nm wavelength against water was checked using a spectrophotometer.

Method of Calculation: The alpha-amylase activity is calculated on dry malt according to the formula:

$$A2 = A1 \times 100 / 100 - M \quad \dots\dots (1)$$

A1 = the amylase activity on sample from the concentration factor; amylase units/mg malt

A2 = the amylase activity on dry malt; amylase units/mg malt; M = moisture content

Production of Glucose Syrup: 250 g of high quality cassava flour, 20 and 40 g of maize grit (milled maize malt) with 10 g calcium carbonate was weighed. Cassava flour, calcium carbonate, 20 g maize grit and 250 ml of water was poured into a beaker and stirred properly for gelatinization and liquefaction. The pH of the mash was checked using a pH meter and was adjusted to 7 using 0.1 NaOH. The mash was poured in a pot and placed on a hot plate. The mash begins to gelatinize. After about 10 min 1.1 L of boiling water was added and boiled for 1 h at high temperature of 95 - 100 °C. The mixture was stirred continuously and cooled to a temperature of 50 °C. The pH of the mash was adjusted using 0.4 M NaOH, and there after mixed thoroughly and placed on the hotplate for 4 h. After 4 h, mixture was poured into beaker and the glucose syrup was made to evaporate and then decanted, the coarse component in it were filtered using filter cloth.



FIG. 4a: FILTRATION SETUP OF OBTAINING GLUCOSE SYRUP FROM THE WORT



FIG. 4b: GLUCOSE SYRUP SAMPLE (MAIZE)



FIG. 4c: GLUCOSE SYRUP SAMPLE (SORGHUM)

Analysis of Glucose Syrup:

Determination of pH: 10 ml of sample syrup was measured into 100 ml beaker and the pH was determined with the aid of a previously standardized pH meter (model Hannap211). The pH meter was calibrated using pH 4.0 and 7.0 buffer.

Determination of Total Solids: 25 ml of each sample was measured into pre-weighed 100 ml beaker. The beakers and the content were placed on a ring water bath for 1 h. The samples were dried in an oven at 105 °C for 2 h, cooled in a desiccator and then weighed on a chemical balance. The percentage total solids were calculated as follows:

$$\text{Total solids} = \frac{W_2 - W_1}{W_2 - W_1} \times 100 \quad \dots\dots (2)$$

Invert Sugar Determination: 2.5 grams of sample was weighed and transferred to 250 ml volumetric flask. 100 ml of neutral lead acetate solution was added and diluted to volumetric water and filtered. An aliquot of 25 ml of the clarified filtrate was transferred to 50 ml volumetric flask containing about 100 ml of water. Potassium oxybate was added in small amount until there is no further precipitation. An aliquot of 50 ml of clarified de-leaded was pipette to a 100 ml volumetric flask, 5 ml of concentrated HCl was also added and allowed to stand at room temperature for 24 h. This was then neutralized with concentrated NaOH solution followed by 0.1N NaOH solution made up to volume and transferred to 50 ml burette having an offset tip to perform the titration in Fehling's solution.

Titration: 5 ml of Fehling solution was put into 250 ml conical flask and was mixed with 10 ml water and a few boiling glass beads. The solution

was dispensed and heated to boiling. 3 drops of methylene blue indicator was added, the addition of solution drop wise was continued until the blue colour disappeared to a brick-red end point. The titre value was recovered, the percentage total reducing sugar (as invert sugar) was calculated as follows:

$$\text{Total Reducing Sugar (as invert sugar)} = \frac{\text{Dilution} \times \text{Fehling factor} \times 100}{\text{Weight of Sample} \times \text{Titre}} \quad \dots\dots (3)$$

Ash Content Determination: 5 g of the crushed sample was weighed into porcelain crucible previously ignited and weighed. Organic matter was charred by igniting the material on a hot plate in the fume cupboard. The crucibles were placed in the muffle furnace and maintained at 600°C. They were then cooled in a desiccator and the content was weighed immediately. The percentage ash content was weighed and calculated as follows:

$$\% \text{ Ash} = \frac{\text{Weight of crucible ash} - \text{Weight of empty crucible}}{\text{Sample weight}} \quad \dots\dots (4)$$

Enumeration of Microorganisms in Glucose Syrup: All glass wares used were properly washed, dried and sterilized in an oven at 180 °C for 3 h.

Media: 23 g of nutrient agar, 52 g mc Conckey agar and 37.9 g of potato dextrose agar were weighed using a digital mettle balance (sutonis) and were suspended into 1 litre (1000 ml) amount of distilled water respectively homogenized on hot plate magnetic stirrer to form a uniform solution.

Diluent: 90 ml and 9 ml distilled water were made in flasks and screw-capped test-tubes for serial dilution. The media and aliquots were sterilized at 121 °C for 15 min in an autoclave. At the end of sterilization period, media were cooled in the water

bath set at 45 °C in order to inhibit bacterial growth. Streptomycin (0.14 g/L (w/v)) was aseptically weighed into potato dextrose agar only for fungi.

Isolation: 10 ml was measured aseptically with a sterile micro pipette and transferred into the first dilution blank of 90 ml distilled water. From the dilution, 1ml was aseptically taken and transferred into the next dilution blank of 9 ml sterile distilled water (10 - 1 dilution). Dispensable petri dishes were set out and labeled accordingly and isolation was carried out using pour plate method. Aliquot (1.0 ml) mcConkey agar (MCA) for chloroforms and potato dextrose sugar agar for fungi respectively in duplicates. The plates were allowed to set and incubated inversely under aerobic conditions at 37 ± 2 °C for bacteria while fungi plates were - incubated at 25 ± 2 °C for 3 - 5 days. The growth on each plate was examined at the end of incubation period, the colony observed on the plates were counted using colony counter. The colony or viable count per ml was calculated by multiplying average number of colonies per countable plate by the reciprocal of the dilution reported as forming units per ml (cfu/ml).

Determination of Soluble Solids (Sugar Brix): A drop of 10% v/v glucose syrup (diluted) was placed on the refractometer eye piece. The refractometer was viewed and the sugar level was read through the graduated mark in the refractometer in degree brix (Brix°).

RESULTS AND DISCUSSION:

Malting Process: Table 1 shows the characteristic feature of grains during steeping. Rice paddy had greatest floating material 33.3 g and maize with no

floating materials. The reason for the high floating material of rice paddy could be as a result of the source of the grains, while maize had no floating materials. Sorghum imbibed most water with a volume of 517.6 ml and rice with lowest of 138.3 ml. Grains were steeped for same duration. The imbibition of water by the grains is due to the different permeability of seed coats of grains. The significance of steeping in malting cannot be overemphasized as this step helps to accelerate the process of germination and increase moisture content of the grains. If the seed coat is impermeable to water or even metals in the soil it can cause imbibition of germination. Germination process allows for the development of endosperm enzymes which helped to modify the starch, proteins and cell walls of the endosperm.

Table 2 above shows maize having the highest germination with green malts weight of 1200 g and lowest as rice with weight of 1000 g. The process employed were in line with the malting procedures as¹⁰. The Grains were allowed to grow under controlled conditions, sugars were produced from grain starch store (which explains a loss of weight when malt is obtained) and natural enzymes developed in the grain kernel. Speed of germination was controlled by temperature, aeration and maintenance of moisture by continued spraying with water. Also turning to avoid grains matting together which was done to obtain good green malt. The reason for kilning is to halt growth and dry grain to stable state at low temperature. Colour and flavor compounds are formed. It is also important to note that rice malt had longest kilning time. Rice malt had lowest yield and can be related to the result of low water imbibition shown in Table 1.

TABLE 1: CHARACTERISTIC FEATURE OF GRAINS DURING STEEPING

Grain	Weight of grains	Weight of floating material	Volume of water	Weight of grains to be steeped	Weight of steeped out grains	Water imbibed during steeping
Rice	900g	33.3g	2 Litres	866.7g	1005g	138.3ml
Sorghum	1000g	7.6g	2 Litres	992.4g	1510g	517.6ml
Maize	1000g	None	2 Litres	1000g	1400g	400ml

TABLE 2: CHARACTERISTIC FEATURE OF MALT FROM CEREAL GRAINS

Cereal grains	Weight of green malt	Weight of dried malt	Weight of clean malt	Malt yield
Rice	1000g	229.8g	194.08g	84.46%
Sorghum	1150g	306g	260g	84.97%
Maize	1200g	530.9	500g	94.33%

Fig. 5 shows maize with greatest malt yield of 94.33% compared to rice with yield of 84.46%.

Sorghum imbibed the greatest volume of water with the highest weight of green malts but did not

give the highest yield of malt. This can be explained by the fact that there are other factors that affect malt yield like the starch store inherent in the grain. Other factors may include: preharvest germination (this is a situation where malting process is stopped meanwhile the grain is still alive), heat damage, contamination during malting, use of immature grains for malting could also reduce the yield of the malt.

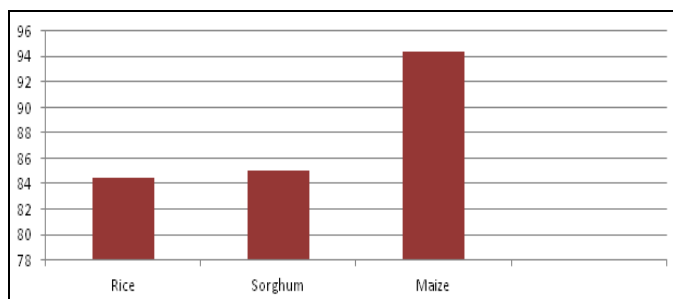


FIG. 5: MALT YIELD OF CEREAL GRAINS

TABLE 3: % MOISTURE CONTENT DURING MALTING FOR 168 h

Duration (h)	Rice (%)	Sorghum (%)	Maize (%)
0	7.58	6.26	6.95
24	7.45	6.43	7.2
48	7.39	6.65	7.31
72	7.66	6.39	7.315
96	7.87	6.53	7.40
120	7.91	6.63	7.47
144	7.98	6.50	7.505
168	7.875	6.43	7.54

Table 3 shows the moisture content during malting. The moisture content for rice malt decreased from 7.58% at the 0th h to 7.39% at the 48th h, this increase continued until the last day of malting; the 168th h with moisture content of 7.875%. For sorghum malt there was fluctuation in the moisture content; constant rise and fall of moisture level until the 120th h with moisture content of 6.63% when there was increase and final drop on the 168th h. The table shows a continuous increase in the moisture content of the maize malt sample from

6.95% at 0th h to 7.54% at the 168th h. High moisture content enhances enzyme production and shoot emergence²².

The amylase activity of the cereal grains are shown in Table 4. The table revealed that amylase unit of the three samples increased throughout the malting process. Amylase activity in rice malt increased from 9.156 in the 0th h to 96.495 on the 168th h, sorghum from 6.311 to 62.519 and maize from 7.706 to 62.519 amylase unit in the 168th h.

TABLE 4: ALPHA-AMYLASE ACTIVITY DURING MALTING (µ/MG MALT)

Duration (h)	Rice	Sorghum	Maize
0	9.156	4.311	7.706
24	16.014	6.636	14.449
48	27.501	10.252	24.077
72	38.229	13.797	38.084
96	55.796	22.807	51.097
120	74.146	33.400	66.421
144	83.371	45.09	82.019
168	96.495	62.519	89.143

Numerous studies of the effect of malting conditions on the production of alpha-amylase have been made and the conclusions reached have agreed quite well^{23, 24, 25} demonstrated that increased steeping moisture, germination time, and germination temperature increased alpha-amylase production. According to²⁶ in their work on exogenous enzymes from sweet potato, Alpha amylase is a liquefying enzyme that drastically reduces the viscosity of gelatinized starch solution to produce mainly maltose, maltotriose, and low molecular weight dextrans. They also stated that amylase brings about complete degradation of starch to metabolize fermentable sugar during germination or malting of cereal grains. The reducing sugar of the grains during malting was as shown in Table 5. The reducing sugar increased with time for rice, sorghum and maize malt respectively.

TABLE 5: REDUCING SUGAR IN MALTED SAMPLE (%)

Duration (h)	Rice		Sorghum		Maize	
	Absorbance at 530nm	Reducing (mg %)	Absorbance at 530nm	Reducing (mg %)	Absorbance at 530nm	Reducing (mg %)
0	0.231	15.59	0.193	13.11	0.241	16.37
24	0.316	24.52	0.261	17.73	0.394	26.77
46	0.493	33.49	0.354	24.05	0.511	34.71
72	0.542	35.59	0.460	31.66	0.667	45.31
96	0.638	43.34	0.611	41.51	0.812	55.16
120	0.741	50.34	0.724	42.51	0.892	60.51
144	0.892	60.59	0.840	54.62	0.842	57.20
168	0.823	55.91	0.804	54.62	0.842	57.20

Change in temperature and pH during malting is shown in **Table 6**. Temperature reduced from 25°C to 18°C for rice malt, decreased from 27°C to 18°C for sorghum malt and finally from 26 °C to 19 °C for maize malt respectively from the beginning of

malting at 0th h to the end at 168th h. The temperature decrease might be as a result of temperature regulation which is done by spraying the malt with water regularly, aeration (air rest), and turning the grain to avoid matting.

TABLE 6: CHANGE IN TEMPERATURE AND pH DURING MALTING

Duration (h)	Rice		Sorghum		Maize	
	T °C	pH	T °C	pH	T °C	pH
0	25°C	6.80	27°C	6.70	26°C	6.85
24	24°C	6.40	26°C	6.50	25°C	6.60
48	24°C	6.10	25°C	6.20	24°C	6.30
72	23°C	5.95	23°C	6.05	23°C	6.10
96	21°C	6.05	22°C	6.00	22°C	6.00
120	20°C	6.15	20°C	5.98	21°C	6.05
144	19°C	6.07	20°C	5.90	20°C	5.98
168	18°C	5.90	18°C	5.85	19°C	5.93

pH for rice malt reduced from 6.80 to 5.95 at the 72nd h but increased at the 96th h and finally decreased to 5.90 at the 168th h. This shows that malt tends toward alkalinity. This also follows for sorghum malt that decreases from 6.70 to 5.85 and maize malt from 6.85 to 5.93 from the 0th hour to 168th h respectively. This research is in line with the fact that pH and temperature influences germination process. Application of an elevated temperature of 22 °C during malting was postulated by some researchers in order to replace the standard temperature of 14°C, as part of the malting technique referred to as “Activated Germination Malting”²⁷. The elevated temperature of 22 °C was intended to cause the activity of the main malt enzymes to appear at earlier stages of steeping of the grain, by fast activation of the embryo. He also stated that Phenomena occurring during malting and mashing depend strongly on the pH value and

temperature. Germination temperature decreases the malt yield and also creates mold growth problems.

This research was free from this effect of malt yield decrease and mold growth because the germination temperature decreased during malting. Volume of glucose syrup samples after filtration was recorded in **Table 7**. Glucose syrup using rice grit after filtration was 707 mL, from sorghum grit 1.02 L and maize grit was 900mL. Hydrolysis using sorghum grit gave the highest yield of glucose syrup, 75.5%. Rice grit gave glucose syrup yield of 52.37% and maize gave 66.67%. Temperature and pH greatly affects the hydrolysis of starch. Other factors that affect yield are type of starch and natural amylase inhibitor. Longer hydrolysis time and high enzyme dose shows highest increment in percentage of glucose yield.

TABLE 7: VOLUME AND YIELD OF GLUCOSE SYRUP PRODUCED

	Cassava starch	Volume of water (mL)		Weight of grit		Weight of CaCO ₃	Volume of glucose syrup after filtration	Glucose syrup yield (%)
		Cold water	Boiling water	Alpha Amylase	Beta Amylase			
Glucose syrup using Rice grit	250g	250 (mL)	1100 (mL)	20g	40g	10g	707mL	52.37(%)
Glucose syrup using Sorghum grit	250g	250 (mL)	1100 (mL)	20g	40g	10g	1020mL	75.55(%)
Glucose syrup using Maize grit	250g	250 (mL)	1100 (mL)	20g	40g	10g	900mL	66.67(%)

Table 8 shows the physiochemical composition of the samples of syrup produced. The composition analyzed were moisture content, ash content, carbohydrate, reducing sugar, total soluble solid, D.E, total reducing sugar and a physical check of

viscosity. Maize sample has the highest moisture content of 15.4%, sorghum sample has highest starch content, maize sample with highest glucose content, rice sample highest D.E during saccharification. Two factors that determine D.E at

the end of liquefaction are dose of amylase added and duration (h) necessary for liquefaction. Ash content from table 8 shows 0.04% for sorghum and 0.01% for maize; which were within 0.03% maximum approved by Standard Organization of Nigeria for ash content specification of glucose syrup. There were no significant difference between the brix values of all the weight ratios used for the production of glucose syrup. The moisture content of the samples were between 15-20% which is the standard by literature.

The percentage conversion to reducing sugars and glucose was computed with rice sample having 85.79%, sorghum sample 83.86% and maize with 82.58. Sorghum is the most viscous of the three samples which were concentrated at the same time and temperature. In addition, rice sample concentrated first during evaporation but it ended up least viscous. The samples were sweet, brown viscous liquid with caramel odour. The factors that could have affected the rate of hydrolysis include: particle size of the malt grit used, and heat applied for the cooking of the starch (cooking of the starch makes it more readily available for enzymatic hydrolysis), natural amylase inhibitor.

The absence of starch in glucose syrup is an indication that amylolytic enzymes involved with liquefaction and saccharification process of starch

during mashing as contained in the malt might have done the process successfully. The mashing process was carried out at a pH of 5.0, for the enzymatic breakdown of starch and protein. Similar pH values of 5.0 - 5.5 was considered adequate for mashing as reported by ²⁸. According to them pH below 4.5 cause a reduction in enzymatic hydrolysis. Final product (Glucose syrup) really depends on amylase/ amylopectin makeup of the starch.

A dark colour was noticed during evaporation in the glucose syrup concentrates, this could result from the application of heat and also the remain of calcium carbonate in the sample. Starch granules naturally contain protein in their structure. The protein content defers depending on the source of starch and is sometimes seen as undesirable since it gives rise to browning reaction during the hydrolysis process to produce the glucose syrup ²⁹. Invert sugar (reducing sugar) contains glucose and fructose. This was as a result of the enzymatic hydrolysis of the solution. Invert sugar was highest in glucose from rice sample and lowest in glucose syrup from maize sample. Invert sugar has a crystal inhibiting (slow down) characteristics and promotes retention of moisture (humectant properties) which means that the shelf life of many products can be extended by the use of Invert Syrup in product formulations.

TABLE 8: PHYSICO-CHEMICAL COMPOSITION OF GLUCOSE SYRUP

Parameter	Syrup sample (Rice)	Syrup sample (Sorghum)	Syrup sample (Maize)
Moisture content (%)	13.80	14.50	15.4
Ash content (%)	0.02	0.04	0.01
Carbohydrate (%)	86.47	84.76	83.05
Reducing sugar			
Fructose (%)	46.29	43.85	42.67
Glucose (%)	40.48	41.24	41.75
Dextrose equivalent (D.E) before evaporation	21	16.5	19
Total soluble solid (Sugar Brix) 100%	100°Brix	110°Brix	105°Brix
Total reducing sugar (Invert sugar) %	85.79	83.86	82.58
Physical check viscosity	Viscous	Most viscous	More viscous
Colour	Brown	Brown	Brown
Taste	Sweet	Sweet	Sweet

Table 9 shows that the 3 samples of glucose syrup are fit for consumption as there were no microbial growth (yeast/molds) present in them. The technology of glucose syrup is complex and the risks of contamination during the processing steps or in the final product are high especially when produced on a large scale. Glucose syrup from

sorghum has the highest total viable count of 5×10^1 (cfu/ml) while rice sample has the lowest with 2×10^1 (cfu/ml). There was no growth of mold or yeast and this was as a result of the high temperature of hydrolysis which made the condition unfavorable for them to survive.

Although, bacterial can grow in the bottles during storage when container is wet and stored in hot places. Risks are also possible due to the external

contamination at mixing, packaging and storage or to the unhygienic manipulation and/or maintenance of equipment.

TABLE 9: MICROBIAL ANALYSIS OF GLUCOSE SYRUP

Sample name	Total viable count in NA (cfu/mL)	Coliform content on MacConkey agar (cfu/mL)	Fungi count Yeast/moulds on PPA (cfu/ml)
Glucose syrup (Rice)	2×10^1	No growth	No growth
Glucose syrup (Sorghum)	5×10^1	No growth	No growth
Glucose syrup (Maize)	3×10^1	No growth	No growth

CONCLUSION: This research developed a very simple and practicable method for the production of glucose syrup from cassava starch with sorghum malt giving the highest yield of glucose syrup of 75.55% and most viscous. This helps to save energy during evaporation. Rice can be used alternatively because of lowest total viable count of 2×10^1 cfu/mL and total reducing sugar (Invert sugar) of 85.79%. Amylase activity of malt was activated which was why the starch was hydrolyzed and glucose syrup obtained.

The research also reviewed that amylase activity of malt increased with malting time until the stored starch is totally consumed. If malting process still continues, amylase activity will fall but if otherwise and kilned the amylase activity is retained.

Amylase activity increases with malting time. Malt yield was compared during malting, total soluble solid, level of concentration after evaporation and other physiochemical composition of the glucose syrup sample, sorghum was most viscous, highest total soluble solid of 110° Brix while rice has the highest D.E of 21 after saccharification and highest percentage of carbohydrate 86.47%.

During hydrolysis, highest concentration of glucose was obtained during 4 hours of operation. This technology demonstrates a good business opportunity to create wealth using available local resources. There is an existing market for glucose syrup in the food and pharmaceutical industries based in Nigeria.

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